

Heat Transport into and out of measuring cells

dimensions :

sides: $50 \times 10 = 500$

ends: $10 \times 8 = 80$

top: $50 \times 8 = 400$

$$Q = \kappa \sum_i (A/d) \Delta T$$

acrylic

$$\kappa = .00033 \text{ T}^{-1.81} \text{ W}/(\text{cm K})$$

at 0.45 K, $\kappa = 8 \times 10^{-5} \text{ W}/(\text{cm K})$;

for 4 mW into single cell, full area, 1 cm wall

$$\sum_i (A/d) \approx 2000 \text{ cm}; \Delta T = 25 \text{ mK}$$

restricting surface area
will result in a problem
for heat flush

time constant

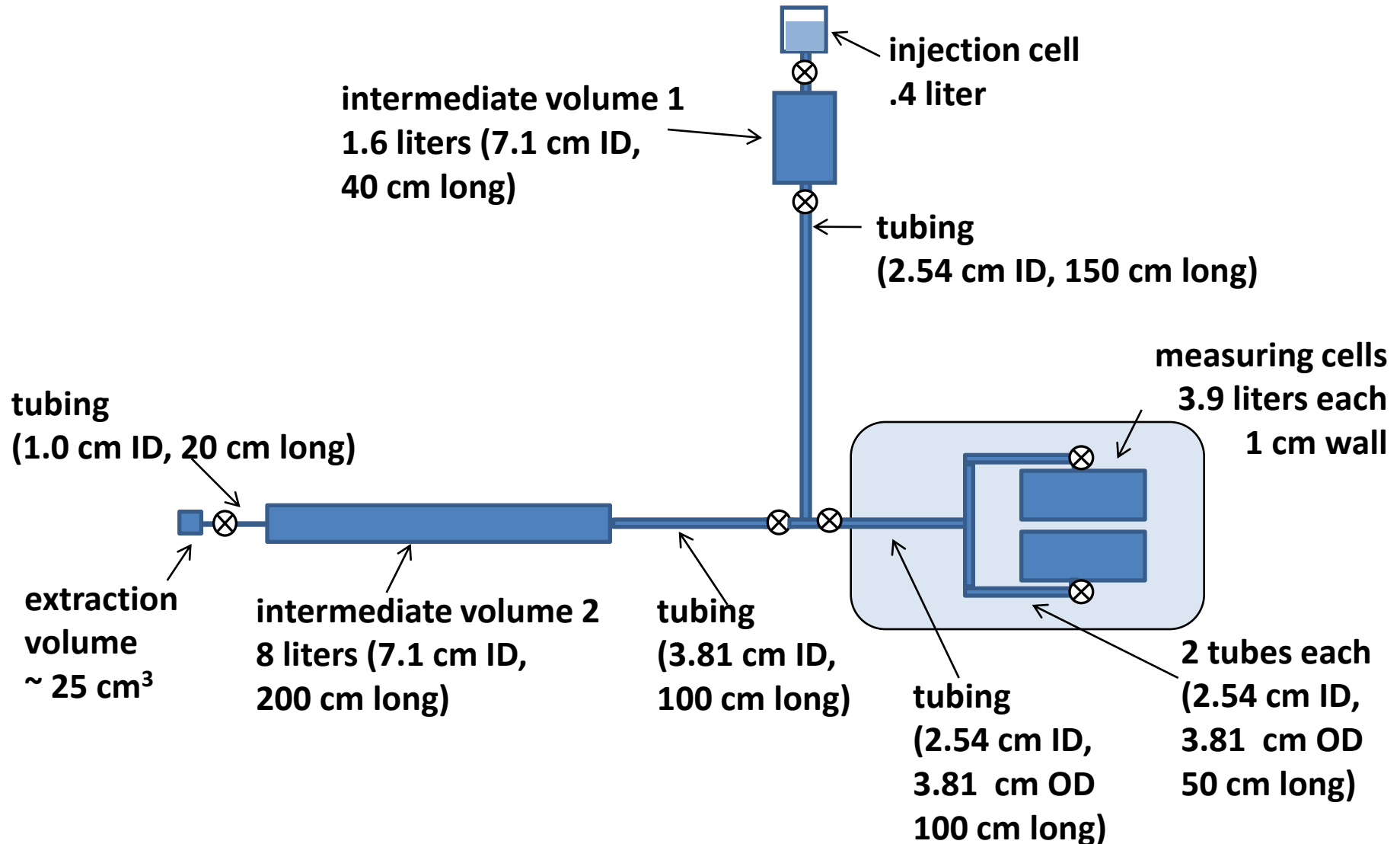
$$\tau = (C/\kappa)(V/\sum_i (A/d))$$

at 0.45 K, $C = 2.4 \times 10^{-4} \text{ J}/(\text{K cm}^3)$

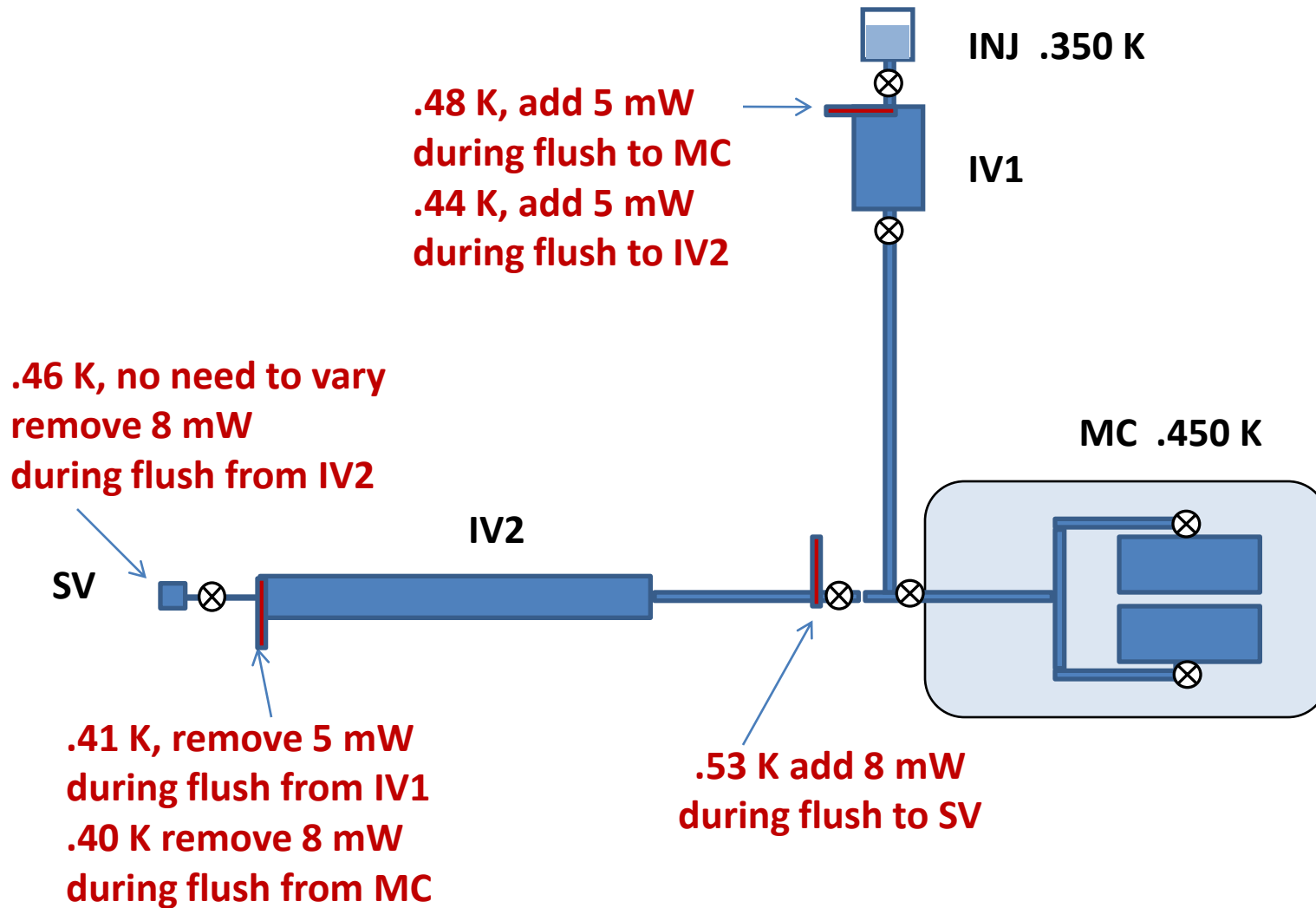
with $V = 4000 \text{ cm}^3$

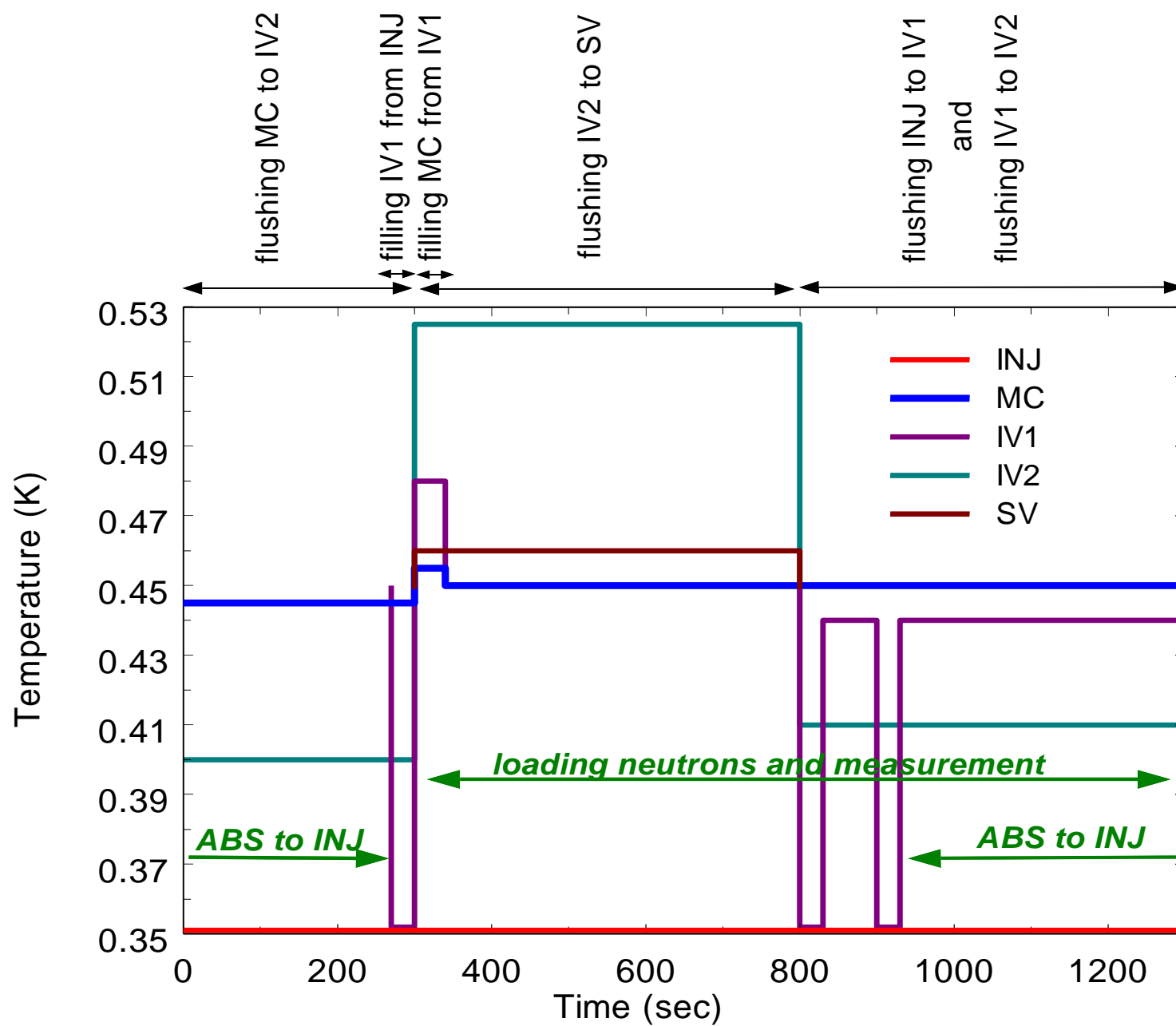
$$\tau = 6 \text{ seconds}$$

schematic of ^3He transport system components and sizes

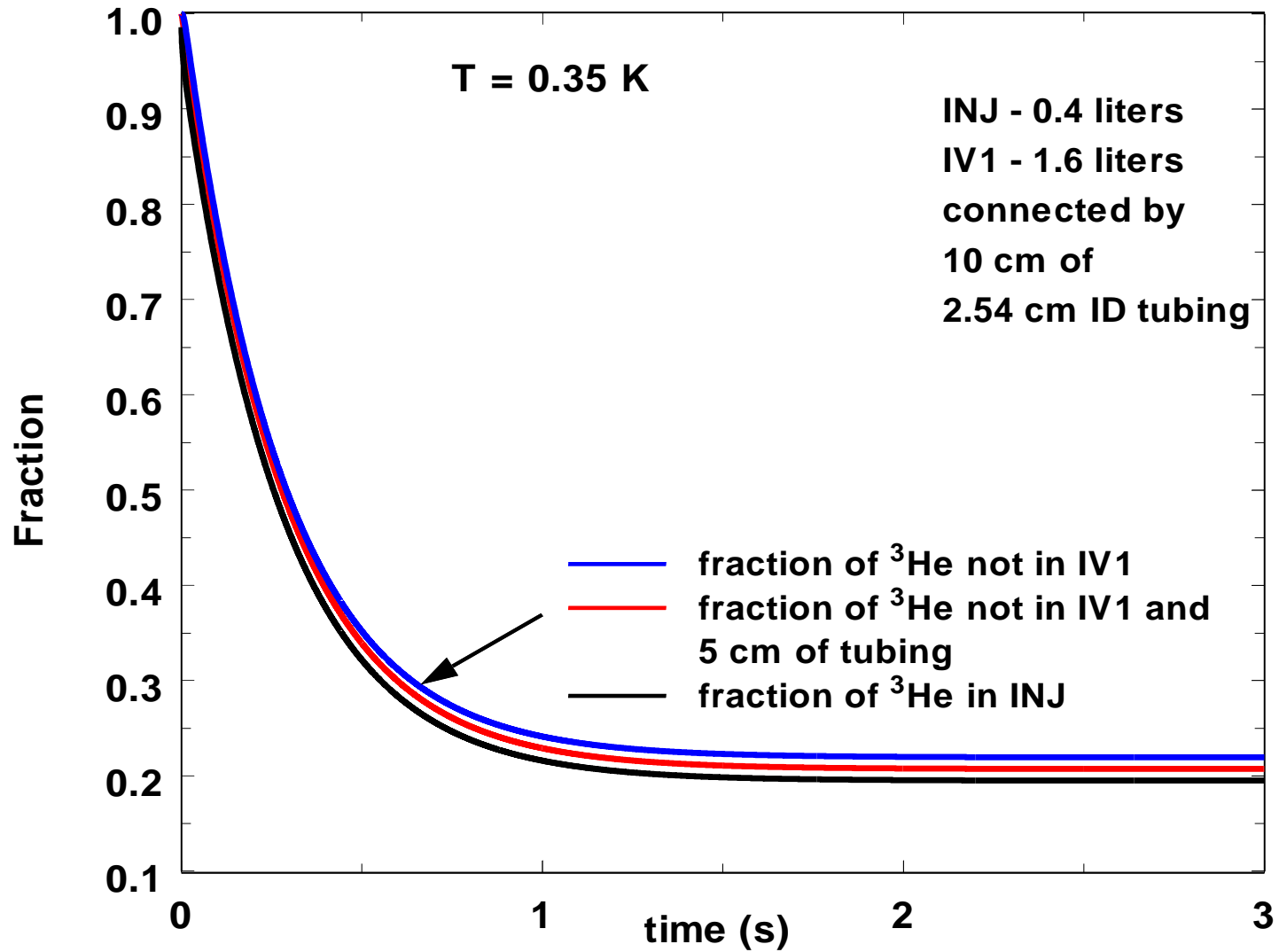


schematic of ^3He transport system temperatures and heat transfers

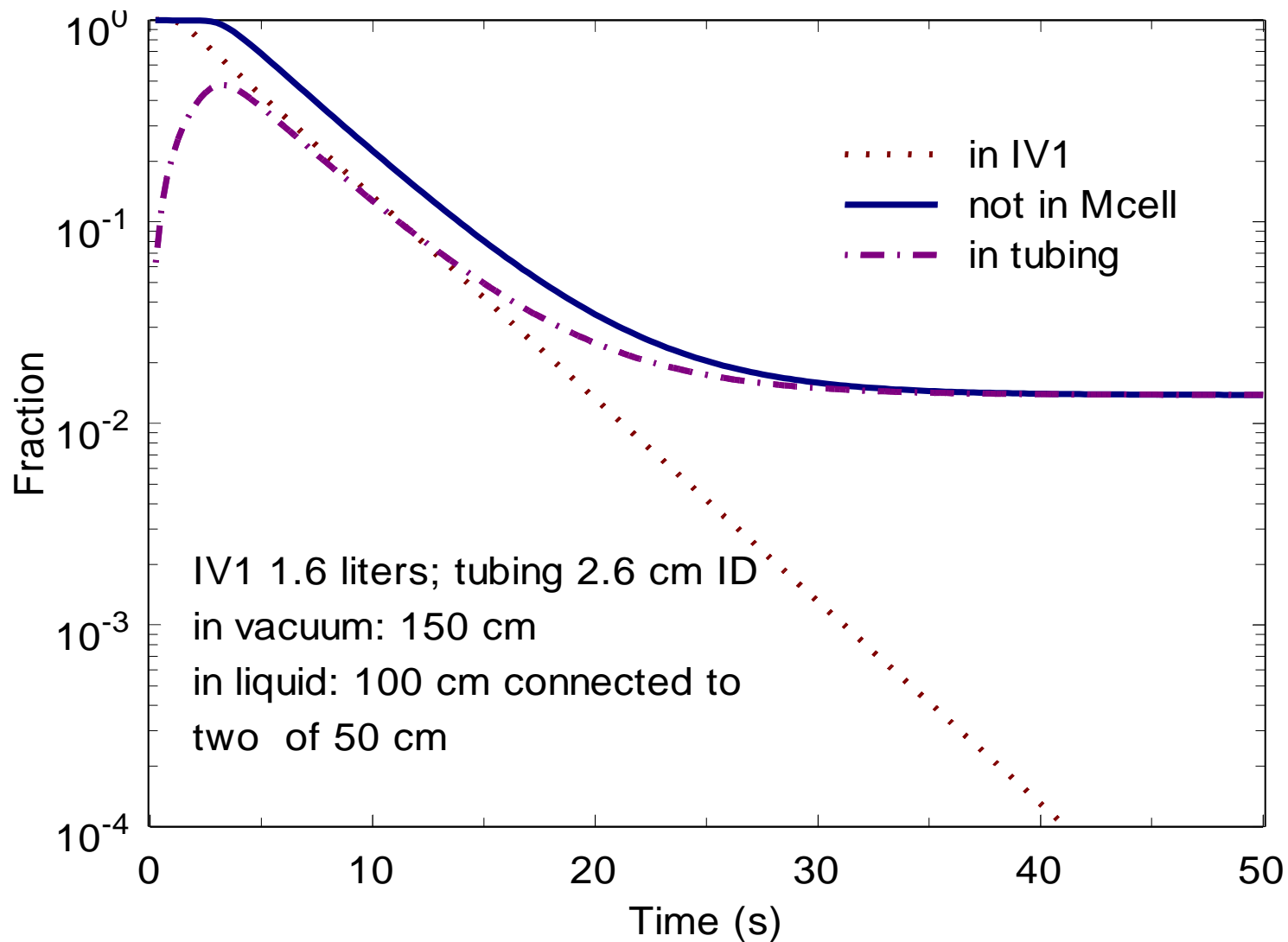




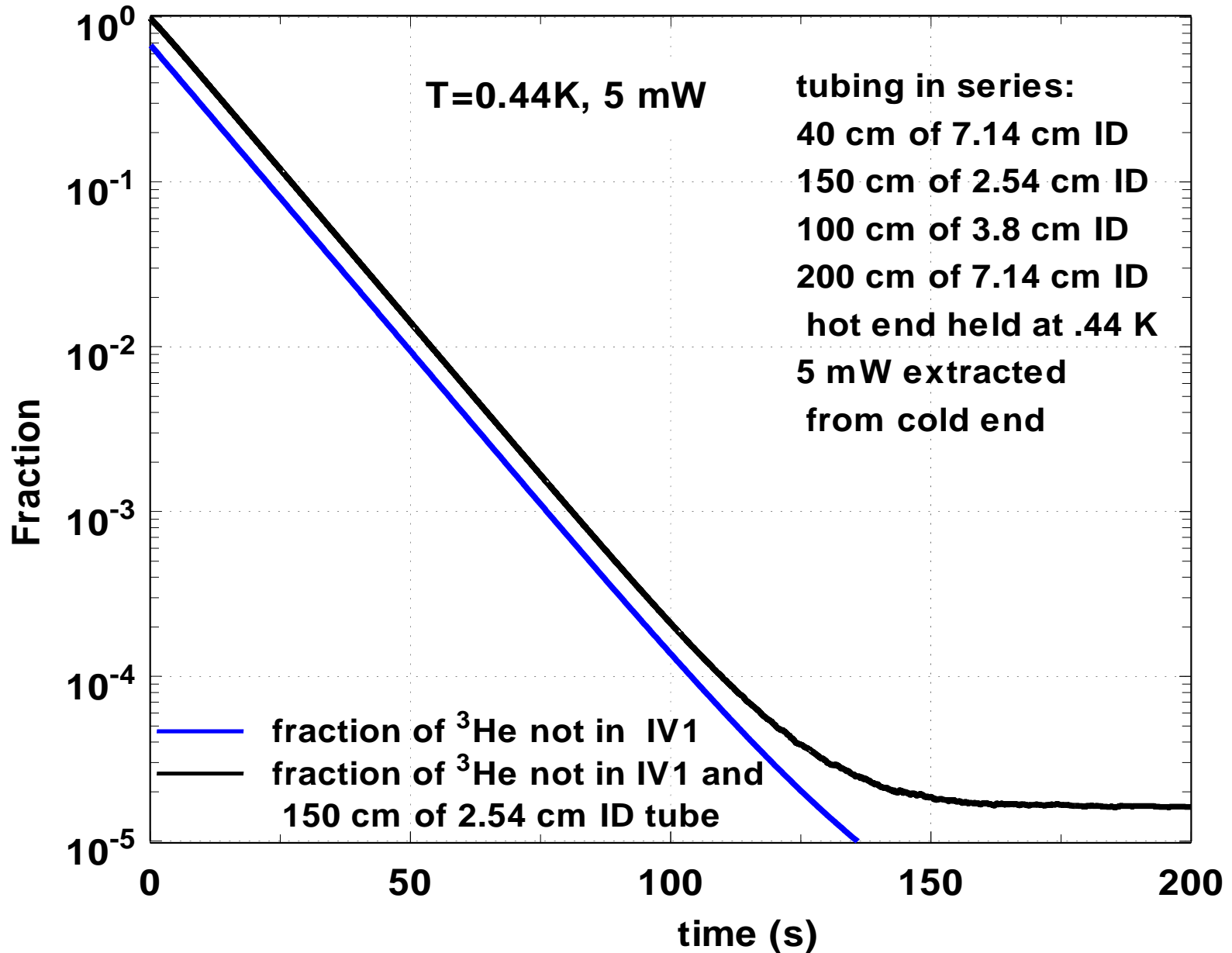
diffusion from injection cell to IV1



Fraction of ^3He in various components: Heat flush from IV1 to Mcell

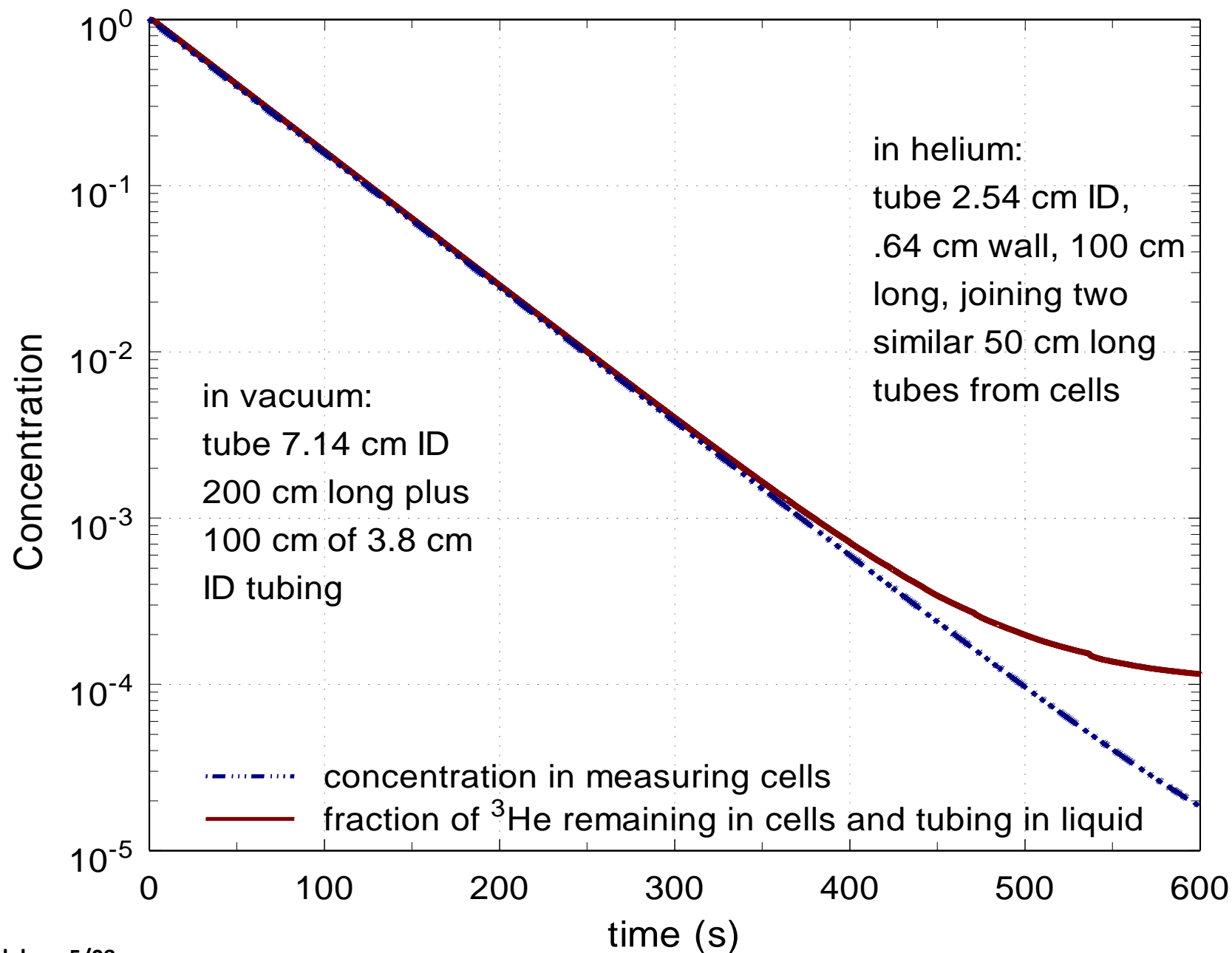


flushing ^3He from IV1 (1.6 Llt) into IV2 (8lit)

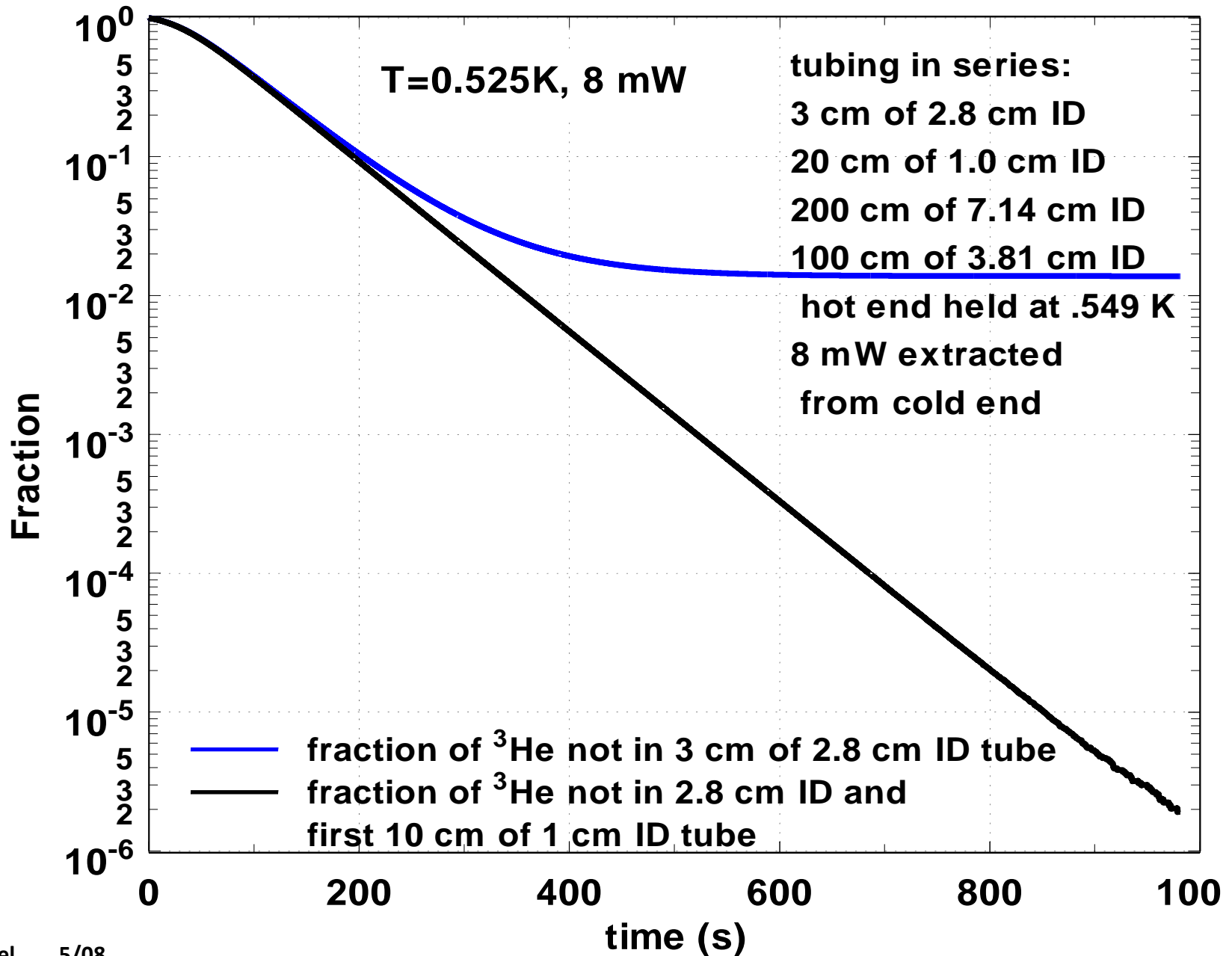


T=0.45K; 8.0 mW

measuring cells 7.75 liters



concentrating ^3He from 8 liter volume into $\sim 25\text{ cm}^3$



removal of liquid with high concentration of ^3He
and
replacement with pure ^4He

transfer liquid via
capillary, 0.05 cm, from
extraction volume to
evaporator
 $\sim 60 \text{ J}$ to evaporate 25 cm^3
recover gas for analysis

heat transfer via helium
in capillaries is small

evaporator
heat above 1 K

